## VALVESTAR® 7 Training-Lectures



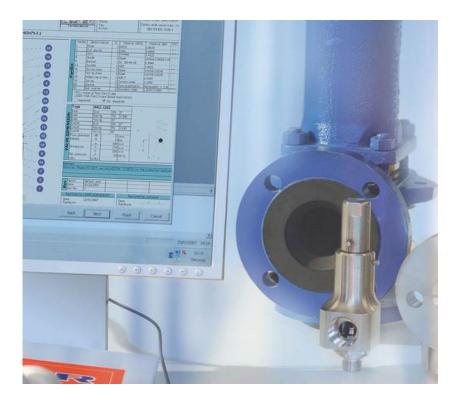


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#### Objectives of this Presentation. Knowledge to learn.

1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

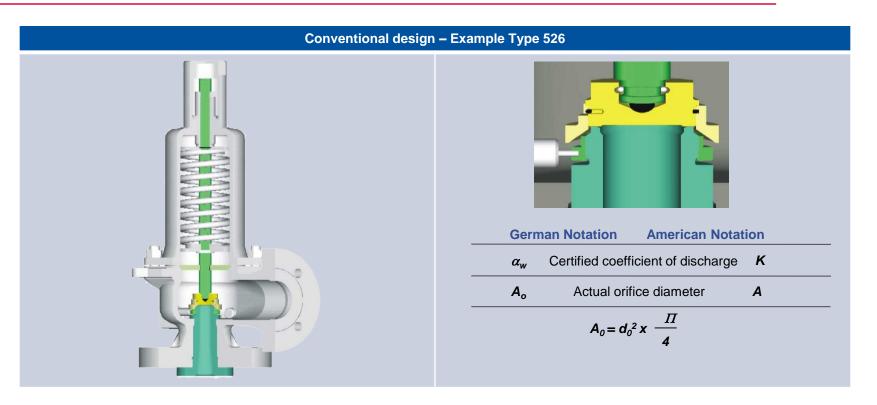
# The aim of the presentation is to inform about training lectures of VALVESTAR<sup>®</sup>7.





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### **Training basics.**





#### **Training Example 1.** Input data – Conventional.

1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

<ul> <li>Medium</li> </ul>	Air
<ul> <li>Set pressure</li> </ul>	10 barg
<ul> <li>Overpressure</li> </ul>	10%
<ul> <li>Temperature</li> </ul>	20 °C
<ul> <li>Required mass flow</li> </ul>	11.500 kg/h
<ul> <li>Body material</li> </ul>	1.0619/WCB
<ul> <li>Lifting device</li> </ul>	Cap H2
<ul> <li>Sizing standard</li> </ul>	DIN EN ISO 4126-7
<ul> <li>LESER Type</li> </ul>	High Performance



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### Training Example 1. Result – Conventional design Type 441.

1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

<ul> <li>Medium</li> </ul>	Air
<ul> <li>Set pressure</li> </ul>	10 barg
<ul> <li>Overpressure</li> </ul>	10%
<ul> <li>Temperature</li> </ul>	20 °C
<ul> <li>Required massflow</li> </ul>	11.500 kg/h
<ul> <li>Body material</li> </ul>	1.0619/WCB
<ul> <li>Lifting device</li> </ul>	Cap H2
<ul> <li>Sizing standard</li> </ul>	DIN EN ISO 4126-7
<ul> <li>LESER Type</li> </ul>	High Performance

ArtNo.	4412.4542
<ul> <li>Certified massflow</li> </ul>	11.882,712 kg/h
<ul> <li>Capacity exceed</li> </ul>	3,33%



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### Training Example 1. Result – Conventional design Type 526.

1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

<ul> <li>Medium</li> </ul>	Air
<ul> <li>Set pressure</li> </ul>	10 barg
<ul> <li>Overpressure</li> </ul>	10%
<ul> <li>Temperature</li> </ul>	20 °C
<ul> <li>Required massflow</li> </ul>	11.500 kg/h
<ul> <li>Body material</li> </ul>	1.0619/WCB
<ul> <li>Lifting device</li> </ul>	Cap H2
<ul> <li>Sizing standard</li> </ul>	DIN EN ISO 4126-7
<ul> <li>LESER Type</li> </ul>	API Series

ArtNo.	5262.2022
<ul> <li>Certified massflow</li> </ul>	11.866,667 kg/h
<ul> <li>Capacity exceed</li> </ul>	3,19%



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## Training Example 2. Additional inlet piping / pressure drop.

<ul> <li>Piping according to</li> </ul>	ISO / CD 4126-9
Inlet length	0,5 m
Inlet diameter	DN 50 / 54,5 mm



## Training Example 2. Result with inlet piping / pressure drop, Type 441.

1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

<ul> <li>Piping according to</li> </ul>	ISO / CD 4126-9
<ul> <li>Inlet length</li> </ul>	0,5 m
<ul> <li>Inlet diameter</li> </ul>	DN 50 / 54,5 mm

<ul> <li>Certified massflow</li> </ul>	11.714,451 kg/h
<ul> <li>Capacity exceed</li> </ul>	1,86%
<ul> <li>Pressure drop</li> </ul>	1,70%



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## Training Example 3. Additional outlet piping / back pressure.

<ul> <li>Piping according to</li> </ul>	ISO / CD 4126-9
<ul> <li>Outlet length</li> </ul>	0,5 m
<ul> <li>Outlet diameter</li> </ul>	DN 80 / 82.5 mm
<ul> <li>Silencer</li> </ul>	p = 0,5 bar



## Training Example 3. Result with outlet piping / back pressure, Type 441.

1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

ISO / CD 4126-9
0,5 m
DN 80 / 82.5 mm
p = 0,5 bar

	Certified massflow	11.714,451 kg/h
•	Capacity exceed	1,86%
	Back pressure ratio	10,90%



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#### Training Example 4. Common specification sheet format.

-		C-2. DATA SHEET of			Doc. No.:		
PRESSURE SAFETY & RELII			IEF VA	LVE	DS-10-018		2 of 12
							H.H.Ly
							Approve
4				106	的相连结论和文		8
5							
		100-PG-035-C/2-12-H		100-	G-036-CA2-	12%H	
				Destate		Chestine .	
						Pressure Reducing Station	
			TOME DEC	***		NOME DEC 1	
			UV			UV	
17	Fiuld		Fuel Gas			Fuel Gas	
18	Phase		Gas			Gas	
19	Required capacity (kg/h) /set	RESERVED	12200	STREET STREET	CARE DE VES	12200	CELEBRATING STATE
		Concernent Ph. Salantel	18.10	LO FORDERAL CONTRACTOR	Constant Constant of the	18.10	Philametria.
21	Density at rollef (kg/m3)		28.76			28.76	
22	Viscosity at relief (cP)		0.01363			0.01363	
23	Operating Pressure (barg)		38			38	
			65			65	
	Set Prossure (barg)	41		41			
26		65		65			
27		1		1			
		100000000000000000000000000000000000000			1. 10. 10. 1. 1.		Access 1
		- which are and the set of the second s				16 20 200	
		ASAM			APRA		150#
	Flange Facing Type (Inlet/Outlet)						
47	Bonnet						
52	Cap (Screwed/Bolted)		Bolted			Bolled	
53	Lifting lever	No		No			
			Yes		Yes		
55			Yes			Yes	
56	1. SWRF type shall be applied for flange size	1/2"-2", and	WNRF type	shail be appl	ed for flange	size 21/2" ar	d over.
57							
58 59							
	Ma Q 5 4 6 6 7 8 9 10 11 12 19 14 15 10 17 18 19 20 12 12 12 12 12 12 12 12 12 12 12 12 12	Marafia IWPP Co: 80701 Safety and Railef Valve 4 Tap.No. 6 Guanty. 7 Banks, and Railef Valve 4 Tap.No. 7 Banks, and Railef Valve 9 Alb No. 7 Banks, and Safety Alb No. 7 B	Marafa WPP         Oc. 180701           Safety and Railer Valve         Safety and Railer Valve           4         Tap No.           5         Guanty.           6         Duanty.           7         Bade States and States	Marafa (WPP)         0           00:80701         0           Safeiy and Railof Valve         REV.           4         Tap No.           6         Guanty.           7         Path No.           9         Path No.           9         Path No.           9         Path No.           9         Path No.           10         Batery valve location           10         Pressure Restudy           10         Path No.           11         Pressure Restudy           12         Declement equipment           13         Declement equipment           14         Cola Vent Sa           15         Cola et ange           16         Accurvation In % of design pressure           16         Cola et ange           17         Fath           18         Cola et ange           19         Design pressure (larg)           10         Accurvatianty           10         Accurvatianty           10         Accurvatianty           10         Accurvatianty           10         Accurvatianty           10         Accurvatianty	Marafig NVPP         0         Are (50), 2007           00:00701         0         Are (50), 2007           8 Guardy         0.1         0.0059000           8 Guardy         1.0         0.0           9 Allo No.         1.0019000000000000000000000000000000000	Marafig NVPP         0         #pt (58,200)         J.B.Jung           Solidiy and Railef Value         REV.         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Fill 1004500.45000         Program         Program           6         Manufacturer         Program         Program         Program         Program           10         Madel No.         Pressure Reducing Station         Pressure           10         Dates value location         Pressure Reducing Station         Pressure           10         Dates value location         Cold Vent Station         Pressure           10         Dates value location         Pressure Reducing Station         Pressure           10         Dates programs         UV         U         Idea           10         Station pressure         UV         Idea         Idea           10         Dates programs         UV         Idea         Idea           10         Dates programs         UV         Idea         Idea           10         Dates program         UV         Idea         Idea <td>Marafiel INVEP     0     Apr. (9)     Apr. (9)     J.S. and Y.       Safety and Relief Valve     REV.     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(9)     20.76       20     Construction In % of design pressure     10.0     23.76     23.76       20     Construction In % of design pressure     10.0     23.76     23.73       20     Construction In % of design pressure     10.0     23.76     23.73       20     Construction In % of design pressure     10.0     23.73     73.73</td>	Marafiel INVEP     0     Apr. (9)     Apr. (9)     J.S. and Y.       Safety and Relief Valve     REV.     DATE     Prepared     Cracked       Safety and Relief Valve     REV.     DATE     Prepared     Cracked       6     Guanty.     F.G. (9)     F.G. (9)     F.G. (9)     F.G. (9)       7.0. PSV. (2004)     F.G. (9)     F.G. (9)     F.G. (9)     F.G. (9)       8     Manuscurve     F.G. (9)     F.G. (9)     F.G. (9)       10     Model No.     Pressure Reducing Bation     Pressure Reducing Iso     Pressure Reducing Iso       11     Pressure Reducing Iso     Pressure Reducing Iso     Pressure Reducing Iso     Pressure Reducing Iso       12     Design pressure     GO2 Vant State     Co3 Vant State     Co3 Vant State       13     Design pressure     UV     UV     UV       14     Accurutation In % of design pressure     F.G. (9)     20.76       20     Construction In % of design pressure     10.0     23.76     23.76       20     Construction In % of design pressure     10.0     23.76     23.73       20     Construction In % of design pressure     10.0     23.76     23.73       20     Construction In % of design pressure     10.0     23.73     73.73



#### Training Example 4. Data from specification sheet.

1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

<ul> <li>Medium</li> </ul>	Fuel Gas: MW = 18,1; Cp/Cv = 1,3739; compressibility factor Z = 0,9405
<ul> <li>Set pressure</li> </ul>	41 barg
<ul> <li>Overpressure</li> </ul>	10%
<ul> <li>Relieving Temperature</li> </ul>	65 °C
<ul> <li>Required massflow</li> </ul>	12200 kg/h
<ul> <li>Body material</li> </ul>	1.0619/WCB
<ul> <li>Lifting device</li> </ul>	Bolted Cap
<ul> <li>Sizing standard</li> </ul>	ASME VIII
<ul> <li>LESER Type</li> </ul>	API Series/Conventional



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#### Training Example 4. Result – conventional design, Type 526.

1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

Fuel Gas: MW = 18,1; Cp/Cv = 1,3739; compressibility factor Z = 0,9405
41 barg
10%
65 °C
12200 kg/h
1.0619/WCB
Bolted Cap
ASME VIII
API Series/Conventional



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### Training Example 4. Result – conventional design, Type 526.

ArtNo.	5262.1452, 2H3,
<ul> <li>Certified massflow</li> </ul>	14.902,653 kg/h
<ul> <li>Capacity exceed</li> </ul>	22,15%



1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation





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- VALVESTAR<sup>®</sup> makes Fire Case sizing according to API RP 521 foolproof.
- In the ASME Boiler & Pressure Vessel Code, Selection VII Div. 1, the protection of pressure vessel in external fire applications is defined. A maximum accumulation of 21% is allowed.
- The sizing equations for external fire applications are specified in API RP 521. The standard differentiates between sizing for the unwetted surface area for gases and wetted surface area for liquids.
- How do you size and select the correct safety valve to protect a pressure vessel filled up with liquid propane with VALVESTAR®? The WIZARD will guide you in 6 steps through this sizing for Fire Vapor generation.



1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

eate new sizing	wizard - !	sizing rype a	nd Medium Selecti	1011					
ing Type and f			g and a medium. Plea	se specify sizing or c	alculation for	a valve. Then s	pecify	a mediu	m and
Tag No.									
Medium		Gas							******
Sizing standard		ASME VIII							
Selected units		ASME VIII							
CDTP Calculation		Ø							
Additional calo	ulations								
						AD2000:A2	AP	1 520	I50 / CD 412
Reaction force									
Noise									
Fire Case								2	
Pressure drop inle	t line								
Built up back pres	sure outlet	pipe							
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#### Step 1: The sizing standard selection

Please select the sizing standard ASME VIII and the extended calculation "Fire Case".

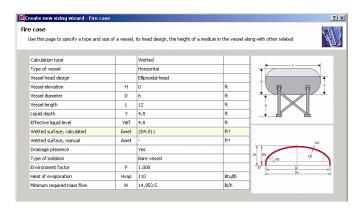
#### Step 2: The medium selection

Please select Propane in the medium database.



1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

Create new sizing wizard	?	×
External Fire Use this page to specify type of effect of fire on the vessel	<b>F</b>	R. C. C.
Effect of Fire on the Wetted Surface of a Vessel	V	
Effect of Fire on the Unwetted Surface of a Vessel		



#### Step 3: The "Wetted Surface Area" sizing

Select the case for FIRE VAPOR GENERATION. This will calculate the amount of vapour generated from the liquid in the protected vessel.

#### Step 4: The calculation of required mass flow

Where adequate draining and firefighting equipment exist, the following equation has to be used.

 $Q = 21,00FA^{0,82}$ 

(API RP 521 Chapter 3.15.2, Equation 3)

Several pieces are necessary to be able to size the required massflow.

Normal liquid level: 80% filled, result: Y = 4,8 ft



1. Objectives | 2. Training basics | 3. Training Example 1 | 4. Training Example 2 | 5. Training Example 3 | 6. Training Example 4 | 7. Fire Case Sizing – vapor evaporation

Maximum allow	able working press	ure					psi-g
Set pressure					p	250	psi-g
Superimposed	hack pressure				paf	0	psi-g
Built up back p					pae		psi
Overpressure					do	21.00	%
Temperature					T	142	op
Required mass	flow				qm,ab	14,953.501	lb/h
	be discharged (wo	rking condition)	1		qvb,at	6,902.24	ft?/h
Volume flow to	be discharged (sto	d condition) [T-	-60 °F P=14.7 ps	0	qvn,at	2,143.685	SCFM
Options							
/ciume flow st	andard				ASME		
Case for blow					Firecase		
Installations	orrection factor					1.000	
ve Selectio	ing wizard - Valv n valve group and the		e from that group.	-			2
ve Selectio rst, choose a Type	n	en any one valv Diameter ran		Body material 1.0619 / SA 2	16 WCB		
Ve Selectio rst, choose a Type 485	n valve group and the d0 13 - 25m d0 23 - 92m	en any one valv Diameter ran N	30 ×	1.0619 / SA 2 Lifting device	16 WCB		
Ve Selectio rst, choose a Type 485	n valve group and the d0 13 - 25mr	en any one valv Diameter ran N		1.0619 / SA 2 Lifting device	16 WCB		
Ye Selectio rst, choose a Type 485 488 Capacity	n valve group and the d0 13 - 25m d0 23 - 92m	en any one valv Diameter ran N	30 ×	1.0619 / SA 2 Lifting device Cap H2	1	escription	
Ye Selectio rst, choose a Type 485 488 Capacity	n valve group and the d0 13 - 25mr d0 23 - 92mr HPS 1 - 61 Certified	on any one valv Diameter ran n Dirfice D - 1	30 ×	1.0619 / SA 2 Lifting device Cap H2	1		
Capacity -6.45 -6.45	n valve group and the d0 13 - 25mr d0 23 - 92mr HPS 1 <sup>1</sup> - 67 Certified massflow [b/h]	Diameter rany n n Orice D - 1 Article No. 5262.0452 5262.0462	20 A	1.0619 / SA 2 Lifting device Cap H2 tiet d0 22.5 22.5	D Type 5262 Orfice G #11 Type 5262 Orfice G #31	50 10 L	
Ve Selectio rst, choose a - Type 485 488 Capacity exceed [%] -6.45 -6.45 -6.45	n valve group and the d0 13 - 25m d0 23 - 92m UPS 1*-61, Certified massflow [b/h] 13,988.559 13,988.559	Diameter rany n n Orineg D - 1 Article No. 5262.0452 5262.0452 5262.0472	30 ▲ DN Inlet × DN out 1 1/2G3 1 1/2G3 1 1/2G3	1.0619 / SA 2           Ufting device           Cap H2           tiet         d0           22.5           22.5	D Type 5262 Orfice G #11 Type 5262 Orfice G #31 Type 5262 Orfice G #31	i0 10 L 10	
e Selectio Type 485 488 Capacity exceed [%] -6.45 -6.45 -6.45	n d0 13 - 25m d0 13 - 25m d0 23 - 92m (02 3 - 92m (05 11-337) Certified massflow ([b/h] 13,988.589 13,988.589 13,988.589	Diameter ran n Article No. 5262.0452 5262.0452 5262.0482	30 A	1.0619 / SA 2 Lifting device Cap H2 tiet d0 22.5 22.5 22.5 22.5	D Type 5262 Orfice G #11 Type 5262 Orfice G #31 Type 5262 Orfice G #31 Type 5262 Orfice G #61	i0 10 L 10	
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Reselection           Type           485           488           300           Capacity           46.45           -6.45           -6.45           -6.45           -6.45           -6.45           -6.45	n valve group and the d0 13 - 25m d0 23 - 92m rP5 1* 8* Cartified massflow [b/h] 13,988.559 13,988.559 13,988.559 13,988.559 13,988.559	Dianeter ran n n Trifice Dr-1 Article No. 5262.0452 5262.0452 5262.0452 5262.0452 5262.0452 5262.0452 5262.0452 5262.0452	20 A	1.0619 / SA 2           Uiting device           Cap H2           tiet         d0           22.5           22.5           22.5           22.5           22.5           22.5           22.5	D Type 5262 Orfice G #11 Type 5262 Orfice G #31 Type 5262 Orfice G #31 Type 5262 Orfice G #31 Type 5262 Orfice G #31	00 L 00 L 00 L 00 L 00 L 00 L 00 L 00 L	
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#### Step 5: The main sizing"

The data for service conditions has to be added to the main calculation according toe ASME VIII.

The required mass flow has been determined by step 4 with the fire case calculation and has been imported into the main calculation.

Set pressure: 250 psig

Saturation temperature: 142 °F

#### Step 6: The selection of safety valve

The WIZARD will then help you in the next steps to select the correct safety valve.

The sizing is finished and can be printed or filed.



# VALVESTAR<sup>®</sup> 7 Thank you for your attention.





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